



Economic Commission for Europe**Inland Transport Committee****Working Party on the Transport of Dangerous Goods****Joint Meeting of Experts on the Regulations annexed to the European Agreement concerning the International Carriage of Dangerous Goods by Inland Waterways (ADN) (ADN Safety Committee)****Twenty-eighth session**

Geneva, 25-29 January 2016

Item 5 (b) of the provisional agenda

**Proposals for amendments to the Regulations annexed to ADN:
Other proposals****Proposal to add to Table C****Transmitted by the Central Commission for the Navigation of the Rhine (CCNR)¹**

1. This question has arisen because it was noted that the various language versions of ADN differed for UN No. 1268 PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S. Following the discussion, it was found that there were similar problems for UN No. 1267 PETROLEUM CRUDE OIL, UN No. 1863 FUEL, AVIATION, TURBINE ENGINE, UN No. 1993 FLAMMABLE LIQUID, N.O.S. and UN No. 3295 HYDROCARBONS, LIQUID, N.O.S. None of the versions were completely coherent.

2. Other problems emerged owing to the wording of remark 38 in Table C, which no longer corresponds with the current content of the requirements. It refers to the conditions applicable for packing group II, while there are already entries for packing group II.

3. The informal working group considered this problem on numerous occasions and concluded that three situations were possible:

(a) Carriage is on a type C vessel. All the data for the calculation of the pressurization of the tank is available. The conditions of transport can be determined using scheme A of the decision tree;

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(b) Carriage is on a type C vessel. Not all the data for the calculation of the pressurization of the tank is available (some is missing). The conditions of transport are determined by referring to ranges of initial boiling points (decision tree, scheme A, fourth column);

(c) Carriage is on a type N closed vessel. The vapour pressure at 50° C determines the conditions of transport (decision tree, scheme B).

4. The method for determining the initial boiling point in accordance with ASTM D 86-01 produces higher values because of the test conditions in the low temperature ranges. This is important from the point of view of safety for initial boiling points near 60° C, the limit for carriage in a pressure tank. That is why for initial boiling points over 60° C and equal to or under 85° C, if the calculation has been done in accordance with ASTM D 86-01, the carriage should just the same be carried out in a pressure tank.

5. For situation (a), above, references are required for packing groups I, II and III, without any information additional to the name or designation. A reference makes it possible to specify that the use of the decision tree is required to determine the conditions of transport.

6. For situation (b) (with data missing), the following references are required:

<i>Packing group</i>	<i>Information additional to the name or designation</i>	<i>Conditions of transport</i>
I	Initial boiling point $\leq 60^\circ \text{C}$	Pressure tank
II	Initial boiling point $\leq 60^\circ \text{C}$	Pressure tank
	$60^\circ \text{C} < \text{initial boiling point} \leq 85^\circ \text{C}$	50 kPa, with water spraying (remark 38)
	$85^\circ \text{C} < \text{initial boiling point} \leq 115^\circ \text{C}$	50 kPa
	Initial boiling point $> 115^\circ \text{C}$	35 kPa
III	Initial boiling point $\leq 60^\circ \text{C}$	Pressure tank
	$60^\circ \text{C} < \text{initial boiling point} \leq 85^\circ \text{C}$	50 kPa, with water spraying (remark 38)
	$85^\circ \text{C} < \text{initial boiling point} \leq 115^\circ \text{C}$	50 kPa
	Initial boiling point $> 115^\circ \text{C}$	35 kPa

7. For situation (c) the following references are required:

<i>Information additional to the name or designation</i>	<i>Conditions of transport</i>
$175 \text{ kPa} \leq P_{d50} < 300 \text{ kPa}$	Pressure tank
$175 \text{ kPa} \leq P_{d50} < 300 \text{ kPa}$	50 kPa with refrigeration
$110 \text{ kPa} \leq P_{d50} < 175 \text{ kPa}$	50 kPa
$110 \text{ kPa} \leq P_{d50} < 150 \text{ kPa}$	10 kPa with water spraying
$P_{d50} < 110 \text{ kPa}$	10 kPa

8. It is proposed to amend the wording of remark 38 in 3.2.3.1, Column (20), which leads to confusion owing to the current content of the requirements, and to recast the remark as follows:

“38. For an initial boiling point above 60° C and under or equal to 85° C as determined in accordance with ASTM D 86-01, the applicable conditions of transport are identical with those stipulated for an initial boiling point under or equal to 60° C.”

9. Furthermore, it is proposed to add to the wording in 3.2.3.3 Column (20) and in 3.2.4.3 L Column (20) so that it reads as follows:

“38. Reference must be made in column (20) to remark 38 for mixtures with an initial boiling point above 60° C or under or equal to 85° C in accordance with ASTM D 86-01.”

10. For Table C it is proposed to delete any mention of UN Nos. 1267, 1268, 1863, 1993 and 3295 and to add the following lines in Table C. Pursuant to the recommendation of the informal working group on substances, “(N1, N2 or N3)” was added to Column (5), “Dangers”, for all entries with the name or designation “WITH MORE THAN 10% BENZENE”.

<i>UN No. or substance identification No.</i>	<i>Name and description</i>	<i>Class</i>	<i>Classification code</i>	<i>Packing group</i>	<i>Dangers</i>	<i>Type of tank vessel</i>	<i>Cargo tank design</i>	<i>Cargo tank type</i>	<i>Cargo tank equipment</i>	<i>Opening pressure of the high-velocity vent valve in kPa</i>	<i>Maximum degree of filling in %</i>	<i>Relative density at 20° C</i>	<i>Type of sampling device</i>	<i>Pump room below deck permitted</i>	<i>Temperature class</i>	<i>Explosion group</i>	<i>Anti-explosion protection required</i>	<i>Equipment required</i>	<i>Number of cones/blue lights</i>	<i>Additional requirements/Remarks</i>
(1)	(2)	(3a)	(3b)	(4)	(5)	(6)	(7)	(8)	(9)	(10)	(11)	(12)	(13)	(14)	(15)	(16)	(17)	(18)	(19)	(20)
1267	PETROLEUM CRUDE OIL	3	F1	I	3+(N1, N2, N3, CMR, F)	*	*	*	*	*	*		*	yes	T4 ³⁾	II B ⁴⁾	yes	*	1	14; *see 3.2.3.3
1267	PETROLEUM CRUDE OIL	3	F1	II	3+(N1, N2, N3, CMR, F)	*	*	*	*	*	*		*	yes	T4 ³⁾	II B ⁴⁾	yes	*	1	14; *see 3.2.3.3
1267	PETROLEUM CRUDE OIL	3	F1	III	3+(N1, N2, N3, CMR, F)	*	*	*	*	*	*		*	yes	T4 ³⁾	II B ⁴⁾	yes	*	0	14; *see 3.2.3.3
1267	PETROLEUM CRUDE OIL WITH MORE THAN 10% BENZENE INITIAL BOILING POINT ≤ 60° C	3	F1	I	3+CMR+F+(N1, N2, N3)	C	1	1		95			1	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	29
1267	PETROLEUM CRUDE OIL WITH MORE THAN 10% BENZENE INITIAL BOILING POINT ≤ 60° C	3	F1	II	3+CMR+F+(N1, N2, N3)	C	1	1		95			1	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	29
1267	PETROLEUM CRUDE OIL WITH MORE THAN 10% BENZENE 60° C < INITIAL BOILING POINT ≤ 85° C	3	F1	II	3+CMR+F+(N1, N2, N3)	C	2	2	3	50	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	23; 29; 38

<i>UN No. or substance identification No.</i>	<i>Name and description</i>	<i>Class</i>	<i>Classification code</i>	<i>Packing group</i>	<i>Dangers</i>	<i>Type of tank vessel</i>	<i>Cargo tank design</i>	<i>Cargo tank type</i>	<i>Cargo tank equipment</i>	<i>Opening pressure of the high-velocity vent valve in kPa</i>	<i>Maximum degree of filling in %</i>	<i>Relative density at 20° C</i>	<i>Type of sampling device</i>	<i>Pump room below deck permitted</i>	<i>Temperature class</i>	<i>Explosion group</i>	<i>Anti-explosion protection required</i>	<i>Equipment required</i>	<i>Number of cones/blue lights</i>	<i>Additional requirements/Remarks</i>
(1)	(2)	(3a)	(3b)	(4)	(5)	(6)	(7)	(8)	(9)	(10)	(11)	(12)	(13)	(14)	(15)	(16)	(17)	(18)	(19)	(20)
1267	PETROLEUM CRUDE OIL WITH MORE THAN 10% BENZENE 85° C < INITIAL BOILING POINT ≤ 115° C	3	F1	II	3+CMR+F+(N1, N2, N3)	C	2	2		50	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	29
1267	PETROLEUM CRUDE OIL WITH MORE THAN 10% BENZENE INITIAL BOILING POINT > 115° C	3	F1	II	3+CMR+F+(N1, N2, N3)	C	2	2		35	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	29
1267	PETROLEUM CRUDE OIL WITH MORE THAN 10% BENZENE INITIAL BOILING POINT ≤ 60° C	3	F1	III	3+CMR+F+(N1, N2, N3)	C	1	1			95		1	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	0	29
1267	PETROLEUM CRUDE OIL WITH MORE THAN 10% BENZENE 60° C < INITIAL BOILING POINT ≤ 85° C	3	F1	III	3+CMR+F+(N1, N2, N3)	C	2	2	3	50	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	0	23; 29; 38

<i>UN No. or substance identification No.</i>	<i>Name and description</i>	<i>Class</i>	<i>Classification code</i>	<i>Packing group</i>	<i>Dangers</i>	<i>Type of tank vessel</i>	<i>Cargo tank design</i>	<i>Cargo tank type</i>	<i>Cargo tank equipment</i>	<i>Opening pressure of the high-velocity vent valve in kPa</i>	<i>Maximum degree of filling in %</i>	<i>Relative density at 20° C</i>	<i>Type of sampling device</i>	<i>Pump room below deck permitted</i>	<i>Temperature class</i>	<i>Explosion group</i>	<i>Anti-explosion protection required</i>	<i>Equipment required</i>	<i>Number of cones/blue lights</i>	<i>Additional requirements/Remarks</i>
(1)	(2)	(3a)	(3b)	(4)	(5)	(6)	(7)	(8)	(9)	(10)	(11)	(12)	(13)	(14)	(15)	(16)	(17)	(18)	(19)	(20)
1267	PETROLEUM CRUDE OIL WITH MORE THAN 10% BENZENE 85° C < INITIAL BOILING POINT ≤ 115° C	3	F1	III	3+CMR+F+(N1, N2, N3)	C	2	2		50	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	0	29
1267	PETROLEUM CRUDE OIL WITH MORE THAN 10% BENZENE INITIAL BOILING POINT > 115° C	3	F1	III	3+CMR+F+(N1, N2, N3)	C	2	2		35	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	0	29
1268	PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S.	3	F1	I	3+(N1, N2, N3, CMR, F)	*	*	*	*	*	*		*	yes	T4 ³⁾	II B ⁴⁾	yes	*	1	14; 27 *see 3.2.3.3
1268	PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S.	3	F1	II	3+(N1, N2, N3, CMR, F)	*	*	*	*	*	*		*	yes	T4 ³⁾	II B ⁴⁾	yes	*	1	14; 27 *see 3.2.3.3
1268	PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S.	3	F1	III	3+(N1, N2, N3, CMR, F)	*	*	*	*	*	*		*	yes	T4 ³⁾	II B ⁴⁾	yes	*	0	14; 27 *see 3.2.3.3

<i>UN No. or substance identification No.</i>	<i>Name and description</i>	<i>Class</i>	<i>Classification code</i>	<i>Packing group</i>	<i>Dangers</i>	<i>Type of tank vessel</i>	<i>Cargo tank design</i>	<i>Cargo tank type</i>	<i>Cargo tank equipment</i>	<i>Opening pressure of the high-velocity vent valve in kPa</i>	<i>Maximum degree of filling in %</i>	<i>Relative density at 20° C</i>	<i>Type of sampling device</i>	<i>Pump room below deck permitted</i>	<i>Temperature class</i>	<i>Explosion group</i>	<i>Anti-explosion protection required</i>	<i>Equipment required</i>	<i>Number of cones/blue lights</i>	<i>Additional requirements/Remarks</i>
(1)	(2)	(3a)	(3b)	(4)	(5)	(6)	(7)	(8)	(9)	(10)	(11)	(12)	(13)	(14)	(15)	(16)	(17)	(18)	(19)	(20)
1268	PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S. WITH MORE THAN 10% BENZENE INITIAL BOILING POINT ≤ 60° C	3	F1	I	3+CMR+F+ (N1, N2, N3)	C	1	1			95		1	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	27; 29
1268	PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S. WITH MORE THAN 10% BENZENE INITIAL BOILING POINT ≤ 60° C	3	F1	II	3+CMR+F+ (N1, N2, N3)	C	1	1			95		1	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	27; 29
1268	PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S. WITH MORE THAN 10% BENZENE 60° C < INITIAL BOILING POINT ≤ 85° C	3	F1	II	3+CMR+F+ (N1, N2, N3)	C	2	2	3	50	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	23; 27; 29; 38

<i>UN No. or substance identification No.</i>	<i>Name and description</i>	<i>Class</i>	<i>Classification code</i>	<i>Packing group</i>	<i>Dangers</i>	<i>Type of tank vessel</i>	<i>Cargo tank design</i>	<i>Cargo tank type</i>	<i>Cargo tank equipment</i>	<i>Opening pressure of the high-velocity vent valve in kPa</i>	<i>Maximum degree of filling in %</i>	<i>Relative density at 20° C</i>	<i>Type of sampling device</i>	<i>Pump room below deck permitted</i>	<i>Temperature class</i>	<i>Explosion group</i>	<i>Anti-explosion protection required</i>	<i>Equipment required</i>	<i>Number of cones/blue lights</i>	<i>Additional requirements/Remarks</i>
(1)	(2)	(3a)	(3b)	(4)	(5)	(6)	(7)	(8)	(9)	(10)	(11)	(12)	(13)	(14)	(15)	(16)	(17)	(18)	(19)	(20)
1268	PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S. WITH MORE THAN 10% BENZENE 85° C < INITIAL BOILING POINT ≤ 115° C	3	F1	II	3+CMR+F+ (N1, N2, N3)	C	2	2		50	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	27; 29
1268	PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S. WITH MORE THAN 10% BENZENE INITIAL BOILING POINT > 115° C	3	F1	II	3+CMR+F+ (N1, N2, N3)	C	2	2		35	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	27; 29
1268	PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S. (NAPHTA) 110 kPa < vp50 ≤ 175 kPa	3	F1	II	3+N2+CMR+F	N	2	3		50	97	0,735	3	yes	T3	II A	yes	PP, EP, EX, TOX, A	1	14; 29

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(1)	(2)	(3a)	(3b)	(4)	(5)	(6)	(7)	(8)	(9)	(10)	(11)	(12)	(13)	(14)	(15)	(16)	(17)	(18)	(19)	(20)
1268	PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S. (NAPHTA) 110 kPa < vp50 ≤ 150 kPa	3	F1	II	3+N2+ CMR+F	N	2	3	3	10	97	0,735	3	yes	T3	II A	yes	PP, EP, EX, TOX, A	1	14; 29
1268	PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S. (NAPHTA) vp50 ≤ 110 kPa	3	F1	II	3+N2+ CMR+F	N	2	3		10	97	0,735	3	yes	T3	II A	yes	PP, EP, EX, TOX, A	1	14; 29
1268	PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S (BENZENE HEART CUT) vp50 ≤ 110 kPa	3	F1	II	3+N2+ CMR+F	N	2	3		10	97	0,765	3	yes	T3	II A	yes	PP, EP, EX, TOX, A	1	14; 29
1863	FUEL, AVIATION, TURBINE ENGINE	3	F1	I	3+(N1, N2, N3, CMR, F)	*	*	*	*	*	*		*	yes	T4 ³⁾	II B ⁴⁾	yes	*	1	14; *see 3.2.3.3
1863	FUEL, AVIATION, TURBINE ENGINE	3	F1	II	3+(N1, N2, N3, CMR, F)	*	*	*	*	*	*		*	yes	T4 ³⁾	II B ⁴⁾	yes	*	1	14; *see 3.2.3.3

<i>UN No. or substance identification No.</i>	<i>Name and description</i>	<i>Class</i>	<i>Classification code</i>	<i>Packing group</i>	<i>Dangers</i>	<i>Type of tank vessel</i>	<i>Cargo tank design</i>	<i>Cargo tank type</i>	<i>Cargo tank equipment</i>	<i>Opening pressure of the high-velocity vent valve in kPa</i>	<i>Maximum degree of filling in %</i>	<i>Relative density at 20° C</i>	<i>Type of sampling device</i>	<i>Pump room below deck permitted</i>	<i>Temperature class</i>	<i>Explosion group</i>	<i>Anti-explosion protection required</i>	<i>Equipment required</i>	<i>Number of cones/blue lights</i>	<i>Additional requirements/Remarks</i>
(1)	(2)	(3a)	(3b)	(4)	(5)	(6)	(7)	(8)	(9)	(10)	(11)	(12)	(13)	(14)	(15)	(16)	(17)	(18)	(19)	(20)
1863	FUEL, AVIATION, TURBINE ENGINE	3	F1	III	3+(N1, N2, N3, CMR, F)	*	*	*	*	*	*		*	yes	T4 ³⁾	II B ⁴⁾	yes	*	0	14; *see 3.2.3.3
1863	FUEL, AVIATION, TURBINE ENGINE WITH MORE THAN 10% BENZENE INITIAL BOILING POINT ≤ 60° C	3	F1	I	3+CMR+F+(N1, N2, N3)	C	1	1		95			1	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	29
1863	FUEL, AVIATION, TURBINE ENGINE WITH MORE THAN 10% BENZENE INITIAL BOILING POINT ≤ 60° C	3	F1	II	3+CMR+F+(N1, N2, N3)	C	1	1		95			1	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	29
1863	FUEL, AVIATION, TURBINE ENGINE WITH MORE THAN 10% BENZENE 60° C < INITIAL BOILING POINT ≤ 85° C	3	F1	III	3+CMR+F+(N1, N2, N3)	C	2	2	3	50	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	0	23; 29; 38

<i>UN No. or substance identification No.</i>	<i>Name and description</i>	<i>Class</i>	<i>Classification code</i>	<i>Packing group</i>	<i>Dangers</i>	<i>Type of tank vessel</i>	<i>Cargo tank design</i>	<i>Cargo tank type</i>	<i>Cargo tank equipment</i>	<i>Opening pressure of the high-velocity vent valve in kPa</i>	<i>Maximum degree of filling in %</i>	<i>Relative density at 20° C</i>	<i>Type of sampling device</i>	<i>Pump room below deck permitted</i>	<i>Temperature class</i>	<i>Explosion group</i>	<i>Anti-explosion protection required</i>	<i>Equipment required</i>	<i>Number of cones/blue lights</i>	<i>Additional requirements/Remarks</i>
(1)	(2)	(3a)	(3b)	(4)	(5)	(6)	(7)	(8)	(9)	(10)	(11)	(12)	(13)	(14)	(15)	(16)	(17)	(18)	(19)	(20)
1863	FUEL, AVIATION, TURBINE ENGINE WITH MORE THAN 10% BENZENE 85° C < INITIAL BOILING POINT ≤ 115° C	3	F1	III	3+CMR+F+(N1, N2, N3)	C	2	2		50	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	0	29
1863	FUEL, AVIATION, TURBINE ENGINE WITH MORE THAN 10% BENZENE INITIAL BOILING POINT > 115° C	3	F1	III	3+CMR+F+(N1, N2, N3)	C	2	2		35	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	0	29
1993	FLAMMABLE LIQUID, N.O.S.	3	F1	I	3+(N1, N2, N3, CMR, F)	*	*	*	*	*	*		*	yes	T4 ³⁾	II B ⁴⁾	yes	*	1	14; *see 3.2.3.3
1993	FLAMMABLE LIQUID, N.O.S.	3	F1	II	3+(N1, N2, N3, CMR, F)	*	*	*	*	*	*		*	yes	T4 ³⁾	II B ⁴⁾	yes	*	1	14; *see 3.2.3.3
1993	FLAMMABLE LIQUID, N.O.S.	3	F1	III	3+(N1, N2, N3, CMR, F)	*	*	*	*	*	*		*	yes	T4 ³⁾	II B ⁴⁾	yes	*	0	14; *see 3.2.3.3

<i>UN No. or substance identification No.</i>	<i>Name and description</i>	<i>Class</i>	<i>Classification code</i>	<i>Packing group</i>	<i>Dangers</i>	<i>Type of tank vessel</i>	<i>Cargo tank design</i>	<i>Cargo tank type</i>	<i>Cargo tank equipment</i>	<i>Opening pressure of the high-velocity vent valve in kPa</i>	<i>Maximum degree of filling in %</i>	<i>Relative density at 20° C</i>	<i>Type of sampling device</i>	<i>Pump room below deck permitted</i>	<i>Temperature class</i>	<i>Explosion group</i>	<i>Anti-explosion protection required</i>	<i>Equipment required</i>	<i>Number of cones/blue lights</i>	<i>Additional requirements/Remarks</i>
(1)	(2)	(3a)	(3b)	(4)	(5)	(6)	(7)	(8)	(9)	(10)	(11)	(12)	(13)	(14)	(15)	(16)	(17)	(18)	(19)	(20)
1993	FLAMMABLE LIQUID, N.O.S. WITH MORE THAN 10% BENZENE INITIAL BOILING POINT ≤ 60° C	3	F1	I	3+(N1, N2, N3, CMR, F)	C	1	1			95		1	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	29
1993	FLAMMABLE LIQUID, N.O.S. WITH MORE THAN 10% BENZENE INITIAL BOILING POINT ≤ 60° C	3	F1	II	3+(N1, N2, N3, CMR, F)	C	1	1			95		1	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	29
1993	FLAMMABLE LIQUID, N.O.S. WITH MORE THAN 10% BENZENE 60° C < INITIAL BOILING POINT ≤ 85° C	3	F1	II	3+(N1, N2, N3, CMR, F)	C	2	2	3	50	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	23; 29; 38
1993	FLAMMABLE LIQUID, N.O.S. WITH MORE THAN 10% BENZENE 85° C < INITIAL BOILING POINT ≤ 115° C	3	F1	II	3+(N1, N2, N3, CMR, F)	C	2	2		50	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	29

<i>UN No. or substance identification No.</i>	<i>Name and description</i>	<i>Class</i>	<i>Classification code</i>	<i>Packing group</i>	<i>Dangers</i>	<i>Type of tank vessel</i>	<i>Cargo tank design</i>	<i>Cargo tank type</i>	<i>Cargo tank equipment</i>	<i>Opening pressure of the high-velocity vent valve in kPa</i>	<i>Maximum degree of filling in %</i>	<i>Relative density at 20° C</i>	<i>Type of sampling device</i>	<i>Pump room below deck permitted</i>	<i>Temperature class</i>	<i>Explosion group</i>	<i>Anti-explosion protection required</i>	<i>Equipment required</i>	<i>Number of cones/blue lights</i>	<i>Additional requirements/Remarks</i>
(1)	(2)	(3a)	(3b)	(4)	(5)	(6)	(7)	(8)	(9)	(10)	(11)	(12)	(13)	(14)	(15)	(16)	(17)	(18)	(19)	(20)
1993	FLAMMABLE LIQUID, N.O.S. WITH MORE THAN 10% BENZENE INITIAL BOILING POINT > 115° C	3	F1	II	3+(N1, N2, N3, CMR, F)	C	2	2		35	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	29
1993	FLAMMABLE LIQUID, N.O.S. WITH MORE THAN 10% BENZENE INITIAL BOILING POINT ≤ 60° C	3	F1	III	3+(N1, N2, N3, CMR, F)	C	1	1			95		1	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	0	29
1993	FLAMMABLE LIQUID, N.O.S. WITH MORE THAN 10% BENZENE 60° C < INITIAL BOILING POINT ≤ 85° C	3	F1	III	3+(N1, N2, N3, CMR, F)	C	2	2	3	50	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	0	23; 29; 38
1993	FLAMMABLE LIQUID, N.O.S. WITH MORE THAN 10% BENZENE 85° C < INITIAL BOILING POINT ≤ 115° C	3	F1	III	3+(N1, N2, N3, CMR, F)	C	2	2		50	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	0	29

<i>UN No. or substance identification No.</i>	<i>Name and description</i>	<i>Class</i>	<i>Classification code</i>	<i>Packing group</i>	<i>Dangers</i>	<i>Type of tank vessel</i>	<i>Cargo tank design</i>	<i>Cargo tank type</i>	<i>Cargo tank equipment</i>	<i>Opening pressure of the high-velocity vent valve in kPa</i>	<i>Maximum degree of filling in %</i>	<i>Relative density at 20° C</i>	<i>Type of sampling device</i>	<i>Pump room below deck permitted</i>	<i>Temperature class</i>	<i>Explosion group</i>	<i>Anti-explosion protection required</i>	<i>Equipment required</i>	<i>Number of cones/blue lights</i>	<i>Additional requirements/Remarks</i>
(1)	(2)	(3a)	(3b)	(4)	(5)	(6)	(7)	(8)	(9)	(10)	(11)	(12)	(13)	(14)	(15)	(16)	(17)	(18)	(19)	(20)
1993	FLAMMABLE LIQUID, N.O.S. WITH MORE THAN 10% BENZENE INITIAL BOILING POINT > 115° C	3	F1	III	3+(N1, N2, N3, CMR, F)	C	2	2		35	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	0	29
1993	FLAMMABLE LIQUID, N.O.S. (CYCLOHEXANONE/ CYCLOHEXANOL MIXTURE)	3	F1	III	3+F	N	3	3		97	0,95		3	yes	T3	II A	yes	PP, EX, A	0	
3295	HYDROCARBONS, LIQUID, N.O.S.	3	F1	I	3+(N1, N2, N3, CMR, F)	*	*	*	*	*	*		*	yes	T4 ³⁾	II B ⁴⁾	yes	*	1	14; *see 3.2.3.3
3295	HYDROCARBONS, LIQUID, N.O.S.	3	F1	II	3+(N1, N2, N3, CMR, F)	*	*	*	*	*	*		*	yes	T4 ³⁾	II B ⁴⁾	yes	*	1	14; *see 3.2.3.3
3295	HYDROCARBONS, LIQUID, N.O.S.	3	F1	III	3+(N1, N2, N3, CMR, F)	*	*	*	*	*	*		*	yes	T4 ³⁾	II B ⁴⁾	yes	*	0	14; *see 3.2.3.3
3295	HYDROCARBONS, LIQUID, N.O.S. WITH MORE THAN 10% BENZENE INITIAL BOILING POINT ≤ 60° C	3	F1	I	3+CMR+ (N1, N2, N3)	C	1	1			95		1	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	29

<i>UN No. or substance identification No.</i>	<i>Name and description</i>	<i>Class</i>	<i>Classification code</i>	<i>Packing group</i>	<i>Dangers</i>	<i>Type of tank vessel</i>	<i>Cargo tank design</i>	<i>Cargo tank type</i>	<i>Cargo tank equipment</i>	<i>Opening pressure of the high-velocity vent valve in kPa</i>	<i>Maximum degree of filling in %</i>	<i>Relative density at 20° C</i>	<i>Type of sampling device</i>	<i>Pump room below deck permitted</i>	<i>Temperature class</i>	<i>Explosion group</i>	<i>Anti-explosion protection required</i>	<i>Equipment required</i>	<i>Number of cones/blue lights</i>	<i>Additional requirements/Remarks</i>
(1)	(2)	(3a)	(3b)	(4)	(5)	(6)	(7)	(8)	(9)	(10)	(11)	(12)	(13)	(14)	(15)	(16)	(17)	(18)	(19)	(20)
3295	HYDROCARBONS, LIQUID, N.O.S. WITH MORE THAN 10% BENZENE INITIAL BOILING POINT ≤ 60° C	3	F1	II	3+CMR+ (N1, N2, N3)	C	1	1			95		1	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	29
3295	HYDROCARBONS, LIQUID, N.O.S. WITH MORE THAN 10% BENZENE 60° C < INITIAL BOILING POINT ≤ 85° C	3	F1	II	3+CMR+ (N1, N2, N3)	C	2	2	3	50	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	23; 29; 38
3295	HYDROCARBONS, LIQUID, N.O.S. WITH MORE THAN 10% BENZENE 85° C < INITIAL BOILING POINT ≤ 115° C	3	F1	II	3+CMR+ (N1, N2, N3)	C	2	2		50	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	29
3295	HYDROCARBONS, LIQUID, N.O.S. WITH MORE THAN 10% BENZENE INITIAL BOILING POINT > 115° C	3	F1	II	3+CMR+ (N1, N2, N3)	C	2	2		35	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	29

<i>UN No. or substance identification No.</i>	<i>Name and description</i>	<i>Class</i>	<i>Classification code</i>	<i>Packing group</i>	<i>Dangers</i>	<i>Type of tank vessel</i>	<i>Cargo tank design</i>	<i>Cargo tank type</i>	<i>Cargo tank equipment</i>	<i>Opening pressure of the high-velocity vent valve in kPa</i>	<i>Maximum degree of filling in %</i>	<i>Relative density at 20° C</i>	<i>Type of sampling device</i>	<i>Pump room below deck permitted</i>	<i>Temperature class</i>	<i>Explosion group</i>	<i>Anti-explosion protection required</i>	<i>Equipment required</i>	<i>Number of cones/blue lights</i>	<i>Additional requirements/Remarks</i>
(1)	(2)	(3a)	(3b)	(4)	(5)	(6)	(7)	(8)	(9)	(10)	(11)	(12)	(13)	(14)	(15)	(16)	(17)	(18)	(19)	(20)
3295	HYDROCARBONS, LIQUID, N.O.S. WITH MORE THAN 10% BENZENE INITIAL BOILING POINT ≤ 60° C	3	F1	III	3+CMR+ (N1, N2, N3)	C	1	1			95		1	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	0	29
3295	HYDROCARBONS, LIQUID, N.O.S. WITH MORE THAN 10% BENZENE 60° C < INITIAL BOILING POINT ≤ 85° C	3	F1	III	3+CMR+ (N1, N2, N3)	C	2	2	3	50	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	0	23; 29; 38
3295	HYDROCARBONS, LIQUID, N.O.S. WITH MORE THAN 10% BENZENE 85° C < INITIAL BOILING POINT ≤ 115° C	3	F1	III	3+CMR+ (N1, N2, N3)	C	2	2		50	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	0	29
3295	HYDROCARBONS, LIQUID, N.O.S. WITH MORE THAN 10% BENZENE INITIAL BOILING POINT > 115° C	3	F1	III	3+CMR+ (N1, N2, N3)	C	2	2		35	95		2	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EP, EX, TOX, A	0	29

<i>UN No. or substance identification No.</i>	<i>Name and description</i>	<i>Class</i>	<i>Classification code</i>	<i>Packing group</i>	<i>Dangers</i>	<i>Type of tank vessel</i>	<i>Cargo tank design</i>	<i>Cargo tank type</i>	<i>Cargo tank equipment</i>	<i>Opening pressure of the high-velocity vent valve in kPa</i>	<i>Maximum degree of filling in %</i>	<i>Relative density at 20° C</i>	<i>Type of sampling device</i>	<i>Pump room below deck permitted</i>	<i>Temperature class</i>	<i>Explosion group</i>	<i>Anti-explosion protection required</i>	<i>Equipment required</i>	<i>Number of cones/blue lights</i>	<i>Additional requirements/Remarks</i>
(1)	(2)	(3a)	(3b)	(4)	(5)	(6)	(7)	(8)	(9)	(10)	(11)	(12)	(13)	(14)	(15)	(16)	(17)	(18)	(19)	(20)
3295	HYDROCARBONS, LIQUID, N.O.S. CONTAINING ISOPRENE AND PENTADIENE, STABILIZED ²	3	F1	I	3+inst.+ N2+CMR	C	2	2	3	50	95	0,678	1	yes	T4 ³⁾	II B ⁴⁾	yes	PP, EX, A	1	3; 27
3295	HYDROCARBONS, LIQUID, N.O.S. (1-OCTEN)	3	F1	II	3+N2+F	N	2	3		10	97	0,71	3	yes	T3	II B ⁴⁾	yes	PP, EP, EX, TOX, A	1	14
3295	HYDROCARBONS, LIQUID, N.O.S. (POLYCYCLIC AROMATIC HYDROCARBONS MIXTURE)	3	F1	III	3+CMR+F	N	2	3	3	10	97	1,08	3	yes	T1	II A	yes	PP, EP, EX, TOX, A	0	14

² Possibly to be added: “60 °C < INITIAL BOILING POINT ≤ 85 °C” Remark 38, consequently with a line for INITIAL BOILING POINT ≤ 60 °C, i.e., pressure tank.